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Originally published:

August 2017

International Journal of Hydrogen Energy 42(2017)33, 20923-20933

DOI: https://doi.org/10.1016/j.ijhydene.2017.07.034

The effect of a Lorentz-force-driven rotating flow on the detachment of gas bubbles from the electrode surface

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Abstract

Water electrolysis is a promising technique for energy conversion and is one of the key technologies to ensure an efficient and clean energy management in the future. However, the efficiency of this process is limited by overpotentials arising from - among other things - the high bubble coverage at the electrode surface. The influence of a magnetic field on the bubble behavior during electrolysis, in particular the bubble detachment from the electrodes, shows great potential for improving the efficiency of the process. In this study experiments and numerical simulations were carried out to investigate the effect of an electrode-normal magnetic field on the bubble detachment. Astigmatism Particle Tracking Velocimetry (APTV) was used to measure the magnetohydrodynamic (MHD) flow field around a magnetized sphere mimicking an electrolytic bubble. Complementary simulations gave further insight into the corresponding pressure field. The experimental and numerical results demonstrate that the pressure reduction formerly assumed to be responsible for the accelerated bubble detachment in the magnetic field is too weak to cause this effect. However, the flow over an arrangement of magnets was additionally measured by Particle Image Velocimetry (PIV), showing that the formation of bubble groups on the electrode surface gives rise to a stronger global flow which may have a substantial influence on the bubble behavior.

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Keywords: electrolysis, magnetohydrodynamics

1. Introduction

Currently, water electrolysis constitutes only 4% of the world hydrogen production, while the major part is generated from fossil fuels [1]. The generation of hydrogen from natural gas is with 1 Euro/kg much cheaper than its production by water electrolysis with approximately 6-10 Euro/kg. However, the possibility to power water electrolysis by renewable energy sources without producing greenhouse gases will eventually make this technique competitive in the future. Moreover, hydrogen is an excellent energy carrier with a high energy density and can be easily reconverted into electrical energy in a fuel cell. Thus, water electrolysis is considered as a key technology for an efficient energy management, which will be important in an energy economy that mainly depends on renewable sources. Among the different electrolyzer types that exist today, alkaline water electrolysis is the most mature and robust technology. It provides long lifetimes and does not rely on expensive cell materials or the need for high temperature handling, which makes this technique currently the most suitable option for the large-scale hydrogen production [2].

The minimum voltage to satisfy the energy demand required for the chemical reactions is referred to as the reversible cell voltage and amounts to $U_{\mathrm{rev}} = 1.23$ V at standard conditions (T = 298.15 K, p = 1 bar). However, in reality additional losses arise due to reaction kinetics at the electrodes and ohmic losses. The cell voltage U_{cell} then calculates to

$$U_{\mathrm{cell}} = U_{\mathrm{rev}} + I \sum R + \Delta U_{\mathrm{anode}} + \Delta U_{\mathrm{cathode}}, \tag{1}$$

with $I \sum R$ accounting for the ohmic losses and $\Delta U_{\mathrm{anode}}$ and $\Delta U_{\mathrm{cathode}}$ denoting the anodic and cathodic overpotential, respectively [3]. Current alkaline water electrolyzers reach efficiencies up to 80-90% for high pressure (30 bar) and elevated temperatures (80 $°C$) [1]. However, for water electrolysis at atmospheric pressure and room temperature the efficiency reaches only 61-79%, depending on the effort taken for improving the performance. Particularly, at high current densities, i.e. high hydrogen production rates, the hydrogen and oxygen gas bubbles that are electrolytically generated at the respective electrodes significantly contribute to these losses, thus limiting the efficiency of the process and the operational current density [4]. As the void fraction in the cell becomes high with increasing current density, the effective conductivity of the bubble-filled electrolyte decreases and causes considerable ohmic losses [5, 6]. On the other hand, since large parts of the electrode

surface are covered by growing gas bubbles, the active electrode area is reduced and the entire current has to pass through the remaining parts of the electrode, which leads to high reaction overpotentials [7, 8]. Therefore, reducing both the electrode bubble coverage and the void fraction is essential to minimize the bubble-related losses and allow for higher efficiencies and hydrogen production rates. It has long been recognized that electrolyte motion can be useful to accelerate the transport of bubbles away from the interelectrode gap, thus decreasing the void fraction and the corresponding ohmic losses [5, 9, 10, 6]. In addition, it also helps to facilitate the bubble detachment and reduce the electrode bubble coverage [11, 12]. A simple and inexpensive method to generate electrolyte motion very close to the electrodes in order to enable an earlier bubble detachment is the application of magnetic fields. The superposition of a magnetic field on the inherent electric field produces Lorentz-forces $\mathbf{F} = \mathbf{j} \times \mathbf{B}$, where $\mathbf{j}$ denotes the current density and $\mathbf{B}$ is the magnetic induction, respectively. These Lorentz-forces act directly as body forces in the fluid (electrolyte) and will generate electrolyte convection if they cannot be balanced by pressure.

The MHD flow generated by electrode-parallel magnetic fields was shown to effectively reduce the void fraction in the interelectrode gap and lower the bubble coverage on large electrodes with increasing magnitude of the magnetic field [13, 14, 15]. Moreover, a reduction of the ohmic losses and overpotentials as well as an improved process performance were reported in the magnetic field [16, 17, 18]. Koza et al. [19, 20, 15] investigated the effect of both an electrode-parallel and electrode-normal magnetic field at large planar electrodes and showed that both configurations were able to reduce the bubble detachment size and the fractional bubble coverage on the electrode. The earlier bubble detachment in an electrode-parallel magnetic field can be attributed to the strong shear flow generated by the Lorentz-forces [21, 22, 23, 24]. However, the underlying mechanisms occurring in an electrode-normal field are currently still under discussion [25, 26]. When an electrode-normal magnetic field is applied, the resulting Lorentz-force is zero in regions where the electric field and the magnetic field are parallel. Now, since a bubble acts as an electric insulator it causes a non-homogeneous current density distribution in its close proximity as schematically shown in Fig. 1 on the left side. This induces Lorentz-forces in azimuthal direction which drive a rotating flow around the bubble. Since the curvature of the electric field lines changes in sign in the lower part, the Lorentz-force will act in opposite direction above and below the bubble's equator. Moreover, the electrical field lines are stronger distorted on the upper part of the bubble, which leads to slightly stronger Lorentz-forces than close to the bottom. Thus, the Lorentz-force-driven rotating flow can be generally expected to be

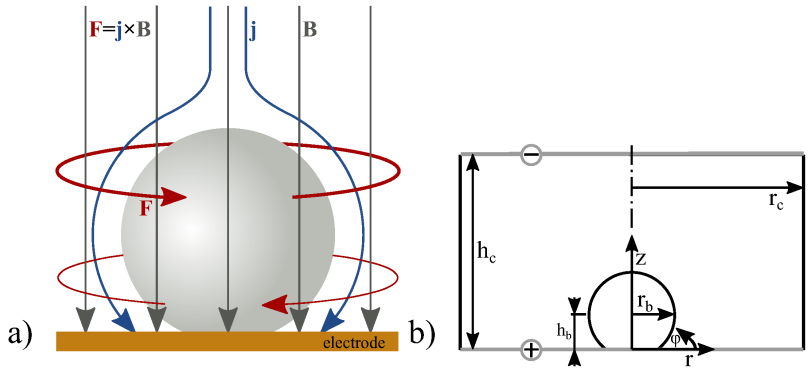

Figure 1: Sketch of the distribution of magnetic induction (**B**), current density (**j**), and Lorentz-force density (**F**) in the vicinity of an electrolytic bubble in an electrode parallel magnetic field (left). Coordinate system and designations of the problem (right).

faster above the bubble equator than below. To explain the faster detachment of the bubbles in such a configuration, it was suggested that the resulting flow forms a region of lower pressure above the bubble. This imposes a force acting in favor of the bubble detachment and thus could explain the reduced detachment size observed in the electrode-normal magnetic field [15].

To pursue this assumption and gain further insight on how to optimize the magnetic field arrangements, a better understanding of the complex three-dimensional flow around the evolving bubbles is necessary. However, it is almost impossible to experimentally investigate the flow around real individual bubbles growing on large electrode since many bubbles may form simultaneously at random places all over the electrode. An alternative approach chosen by many researches is to use nano- [27] or microelectrodes (diameter $\sim O(100\,\mu\mathrm{m})$) in order to pin the bubbles at a certain position which can be investigated by optical means [26, 28, 29, 30, 31]. In contrast to the observations at large electrodes, the experimental and numerical results reported in these studies point to a stabilizing effect of the electrode-normal magnetic field, i.e. an increase of the detachment size. The opposite behavior can be attributed to the strong difference of the Lorentz-force distribution. Since the entire current has to pass through the much smaller microelectrode, the current density and the Lorentz-forces are much stronger at the bottom than at the top of the bubble. This gives rise to a lower pressure in the lower part of the bubble as opposed to the case at large electrodes and may explain the stabilizing effect [26, 25]. Nonetheless, the reported gas bubble behavior on microelectrodes cannot be directly transferred to the realistic case of gas bubbles on macroelectrodes as the Lorentz-force distributions in both cases

are by no means comparable.

The aim of the current study is to provide further insight into the complex MHD flow generated by an electrode-normal magnetic field and clarify the effect of the hydrodynamic force on the bubble detachment at large electrodes. Since the bubbles form at random places it is not possible to conduct detailed flow measurements around a single bubble at a large electrode, therefore a magnetized sphere is used here instead. This setup enables to mimic a single stationary electrolytic gas bubble on a macroelectrode with an equivalent Lorentz-force distribution. The three-dimensional electrolyte flow around the magnetic sphere was experimentally resolved using Astigmatism Particle Tracking Velocimetry for the first time. These measurements are supported by additional numerical simulations, which allowed for the calculation of the hydrodynamic forces that are imposed on the sphere or bubble by the MHD flow. In addition, Particle Image Velocimetry (PIV) measurements were conducted in a second setup employing an arrangement of multiple magnets in order to study the global MHD flow that is formed in the case of bubble groups as opposed to single bubbles.

2. Experimental setup

Given the rotational symmetry of the MHD flow around a single sphere in an electrode-normal magnetic field (see Fig. 1 right), a cylindrical electrolysis cell with an inner diameter of 35.6 mm was used for the measurements as shown in Fig. 2. The cell was made from Plexiglass to allow for optical access from the side walls. The working electrode consists of pure copper and formed the bottom of the cell, whereas a Cu ring electrode placed on the top of the cell served as counter electrode. This allowed for an undisturbed observation of the measurement volume from the top. At the bottom of the cell an axially magnetized NdFeB sphere with a diameter of 10 mm was placed onto a plastic pillar with a height of 8 mm. Using this magnetized sphere the same Lorentz-force distribution as in the case of a stationary spherical gas bubble at a large electrode in an electrode-normal magnetic field can be generated as will be explained in the following. The magnetic field in an infinite domain outside ($r > r_\mathrm{b}$) of a spherical magnet with magnetization M_0 is given by [32]

$$\begin{aligned} B_r &= \frac{2}{3} M_0 \frac{r_\mathrm{b}^3}{r^3} \cos\theta \\ B_\theta &= \frac{1}{3} M_0 \frac{r_\mathrm{b}^3}{r^3} \sin\theta \end{aligned} \tag{2}$$

Here, r, θ, φ are spherical coordinates originating at the center of the sphere and r_b is the radius of the sphere. Similarly, the electric field around a

spherical insulator in an infinitely extended space can be written as [33]

$$\begin{aligned} E_r &= E_0 \left(1 - \frac{r_\mathrm{b}^3}{r^3}\right) \cos\theta \\ E_\theta &= -E_0 \left(1 + \frac{r_\mathrm{b}^3}{2r^3}\right) \sin\theta \end{aligned} \tag{3}$$

From Eq. (2) and Eq. (3) the Lorentz-force distribution around an electrically insulating spherical magnet results as

$$f_{L,\mathrm{M}} = \sigma_e \mathbf{E} \times \mathbf{B} = \sigma_e E_0 M_0 \frac{r_\mathrm{b}^3}{r^3} \sin\theta \cos\theta \ \mathbf{e}_\varphi \tag{4}$$

On the other hand, the Lorentz-force distribution around and insulating (and non-magnetic) sphere in an uniform vertical magnetic field B_z follow as

$$f_{L,\mathrm{B}} = -\frac{3}{2} \sigma_e E_0 B_z \frac{r_\mathrm{b}^3}{r^3} \sin\theta \cos\theta \ \mathbf{e}_\varphi. \tag{5}$$

Note that the Lorentz-force distributions solely possess an azimuthal (φ) component and for both cases differ only by a constant factor. Identical Lorentz-force distributions for $f_{L,\mathrm{M}}$ and $f_{L,\mathrm{B}}$ result if

$$B_z = -\frac{2}{3} M_0 \tag{6}$$

However, to ensure the same Lorentz-force distribution as for the case of an insulating sphere the magnetic sphere could not be placed directly on the electrode but had to be lifted from the ground. The Lorentz-force distribution is generally confined to the vicinity of the sphere, although the ring electrode also creates strong distortions of the current field in the upper part of the cell. The magnetic field is already very weak in this region and thus the generated Lorentz-forces can be neglected. Since the elevated magnetic sphere cannot account for the effect of the bottom wall, the case of an insulating sphere directly attached to the electrode will be additionally considered in a second set of numerical simulations (see Sec. 3).

The cell was filled with a 1 M Cu_2SO_4 solution as an electrolyte, which ensured in conjunction with the pure copper electrodes that a current field is established even below the decomposition voltage of water. It should be mentioned that local density gradients will be created in the electrolyte with time due to the dissolution and deposition of copper. However, since the bottom electrode was used as the anode, copper was only dissolved at the bottom of the cell, which leads to a stable stratification. The experiments

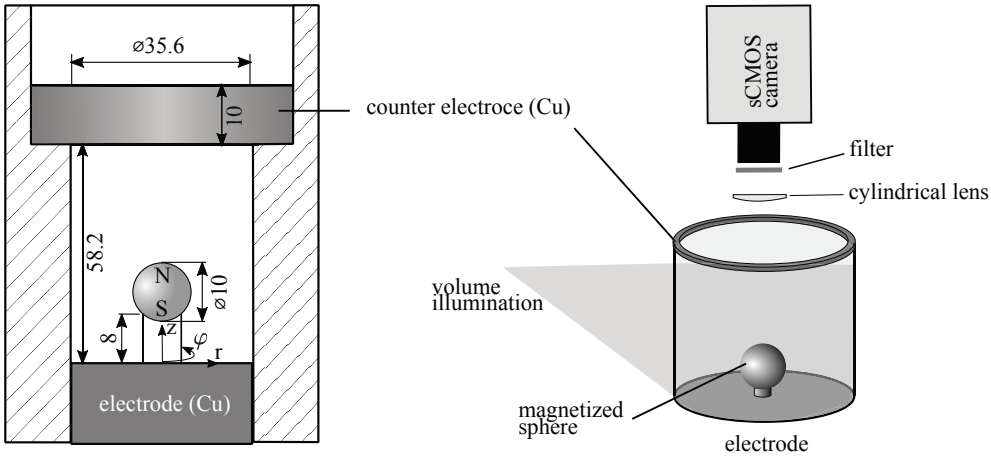

Figure 2: Sketch of the electrochemical cell employing a magnetized sphere (left) and the corresponding APTV measurement setup (right).

were carried out under galvanostatic conditions, i.e. using a constant current supply. Different values of the electric current were applied in successive experiments in order to vary the magnitude of the Lorentz-force ($f_L \sim jB$). Here, a current of $I = 30$, 60, 90, 120 and 150 mA was used, which yields a current density at the surface of the working electrode of about $j = 30$, 60, 90, 120 and 150 $\mathrm{Am^{-2}}$. The magnetization of the sphere amounts to 1 T, thus generating a Lorentz-force distribution that is equivalent to that induced by an uniform electrode-normal magnetic field of $B_z = 0.66$ T according to Eq. (6). Altogether, the magnitude of the resulting Lorentz-forces is in good agreement with the experiments by Koza et al. [15].

A sketch of the experimental setup is shown on the right side of Fig. 2. All three components of the three-dimensional velocity field (3D3C) around the elevated magnetized sphere were measured by means of Astigmatism Particle Tracking Velocimetry [APTV, see 34]. This is a special single-camera particle tracking technique in which a cylindrical lens is placed in front of the camera to disturb the axis-symmetry of the optical system and causes astigmatic aberrations. The particle images will appear elliptical, where the size of the major and minor axes unambiguously depend on the actual depth position in the measurement volume. By a proper image processing and calibration this can be correlated with the actual depth position of the particle [35]. Fluorescent polystyrene particles (FluoRed by Microparticles GmbH) with a diameter of 50 μm served as flow tracers. Even though these particles are relatively large, they do not suffer from fast sedimentation, since their density is very close to that of the electrolyte ($\rho_{\mathrm{Cu_2SO_4}} \approx 1.05\,\mathrm{gcm^{-3}}$, $\rho_{\mathrm{particle}} \approx 1.06\,\mathrm{gcm^{-3}}$). A pulsed Nd:Yag laser with a wave length of 532 nm

and a pulse energy of 15 mJ was used as a light source. The laser beam was passed through a beam expander via an optical fiber and illuminated the entire cell. The images were captured from the top at a frame rate of 15 Hz by a sCMOS camera (Imager sCMOS, LaVision GmbH) and a Zeiss f = 50 mm macro-planar objective. Two laser pulses without time delay were shot in each frame, to increase the illumination intensity. A 532 nm notch filter was mounted on the objective to only transmit the fluorescent light emitted by the tracer particles and avoid the strong laser reflections from the copper surface. Moreover, a cylindrical lens with a focal length of f = 300 mm was placed in front of the camera to create astigmatic distortions of the particle images. The resulting measurement volume extended over the entire inner diameter of the electrolysis cell, from the bottom of the cell ($z = 0\,\mathrm{mm}$) to a height of $z \approx 40\,\mathrm{mm}$. The velocity was reconstructed from the three-dimensional particle positions by determining the particle trajectories with a time-resolved tracking algorithm. Moreover, the trajectories were locally fitted by a second order polynomial fit for a higher accuracy [36]. Since the MHD flow is steady and rotationally symmetric, the velocity data was averaged over the whole circumference into one meridional (rz) plane. The corresponding bin size was $0.5 \times 0.5\,\mathrm{mm}^2$.

3. Numerical Simulations

The finite volume library OpenFOAM licensed under the GNU General Public Licence [37] was used to perform the computations. To incorporate the electromagnetic body force, the solver simpleFoam of OpenFOAM version 1.7.x was extended by a Lorentz-force term. Under the conditions considered here, this term can be pre-computed and does neither depend on time nor on the flow. This is not immediately clear from Ohm's law for moving conductors

$$\mathbf{j} = \sigma(\mathbf{E} + \mathbf{v} \times \mathbf{B}) \tag{7}$$

that - besides the conventional proportionality to the electric field $\mathbf{E}$ - relates the current density to an induction term $\mathbf{v} \times \mathbf{B}$ depending on velocity $\mathbf{v}$ and magnetic field $\mathbf{B}$. However, the electrolyte's electrical conductivity σ is quite small and velocities as well as magnetic field magnitudes are moderate. For this reason, the electric currents induced by the electrolyte motion and even more so the magnetic fields of the induced currents can safely be neglected compared to the applied electric and magnetic fields. Therefore, the calculation of the Lorentz-forces can be decoupled from solving the Navier-Stokes equations.

Current distributions were always determined numerically in order to account for additional insulating parts such as the pillar tethering the sphere,

even if the analytical expression was used for the magnetic field of the magnetized sphere. The electric field $\mathbf{E}$ was computed by solving a Laplace equation for the electric potential using the OpenFOAM solver laplacianFoam. Fixed potentials were set at the top and the bottom of the cell such as to match the desired cell current. The vertical boundaries as well as the bubbles surface were treated as insulating, i.e., no normal currents were allowed there. The current density distribution then results simply from the gradients of the electric potential times conductivity.

Two slightly different setups were used for the comparison with the experiment (Figs. 4, 5) on the one hand and to determine the scaling of the forces (Fig. 6) on the other hand. That means, the first configuration is based on the experiment using the tethered magnetized sphere as discussed in the previous section. Validated by the experimental data, these simulations formed the groundwork for the computation of the more bubble-growth-like case of an insulating sphere that is directly attached to the electrode. This way, the effect of the electrode on the current distribution and the influence of the solid wall on the flow can also be accounted for. For the latter case, a homogeneous magnetic field in vertical direction was combined with the electric field obtained from the Laplace equation.

In both cases, the two-dimensional Navier-Stokes equations with body force term were solved on an axis-symmetric structured grid. A mesh with approximately 2.5×10^5 hexahedral cells and highest resolution in the vicinity of the sphere was used for the tethered sphere geometry of Fig. 2. The parameter studies depicted in the right diagram of Fig. 6 were conducted under the assumption of a constant aspect ratio between cell and bubble, while the cell radius amounted to four times the bubble radius and the cell height was twelve times the radius of the bubble.

4. Results and discussion

4.1. Forces

The detachment of the bubble from the electrode surface depends on the forces that are acting on it. The prevailing forces that are usually considered in this context are the buoyancy F_B, the surface tension force F_γ and the hydrodynamic forces, here referred to as $F_{\Delta p}$ (see Fig. 3). The buoyancy force acts in favor of the the bubble detachment and increases with the bubble size according to

$$F_{Bz} = (\rho_l - \rho_g)\, V\ g = (\rho_l - \rho_g)\, \frac{\pi}{6} d^3\ g, \tag{8}$$

where ρ_g and ρ_l, are the density of the gaseous phase (bubble) and the liquid phase (electrolyte), respectively, V denotes the bubble volume, d is the bubble

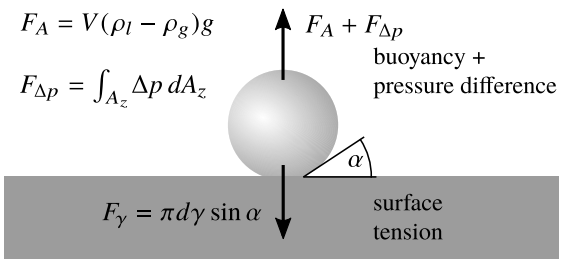

Figure 3: Sketch of the forces acting on a bubble at a horizontal electrode.

diameter and g the gravitational acceleration. The surface tension force F_γ, on the other hand, is responsible for keeping the bubble attached to the surface. For the simple case of a bubble adhering to a horizontal surface in a rotationally symmetric flow, the resulting force can be written as

$$F_{\gamma z} = -\pi d_c \gamma \sin\alpha, \tag{9}$$

where α denotes the contact angle, γ is the gas-liquid surface tension and d_c is the contact diameter of the bubble with the wall,

Since a stationary sphere is considered here, no hydrodynamic drag is imposed. The only relevant hydrodynamic force that needs to be considered in the present case is related to the MHD-induced relative pressure change along the surface of the sphere, which yields for the z-direction

$$\mathbf{F_{\Delta p}} = -\int_{A_z} (p_l - p_c) dA_z, \tag{10}$$

where $\Delta p = p_l - p_c$ is the hydrodynamic pressure of the liquid relative to the reference pressure at the contact line and A_z is the bubble surface projected in z-direction. In a stagnant liquid the bubble will generally stay attached to the surface until the bubble size and thus its buoyancy becomes sufficiently large to overcome the surface tension force. In the presence of an electrode-normal magnetic field, the MHD-induced pressure force $F_{\Delta p}$ might facilitate its detachment. Based on the numerical results $F_{\Delta p}$ will be compared to the buoyancy force F_B in order to asses the effect of the MHD-induced pressure change on the bubble detachment.

4.2. Flow fields

The flow fields are qualitatively very similar for the different investigated currents. Therefore, only the flow field at $I = 60\,\mathrm{mA}$ is considered here for a detailed discussion. Fig. 4 shows all three mean velocity components in the

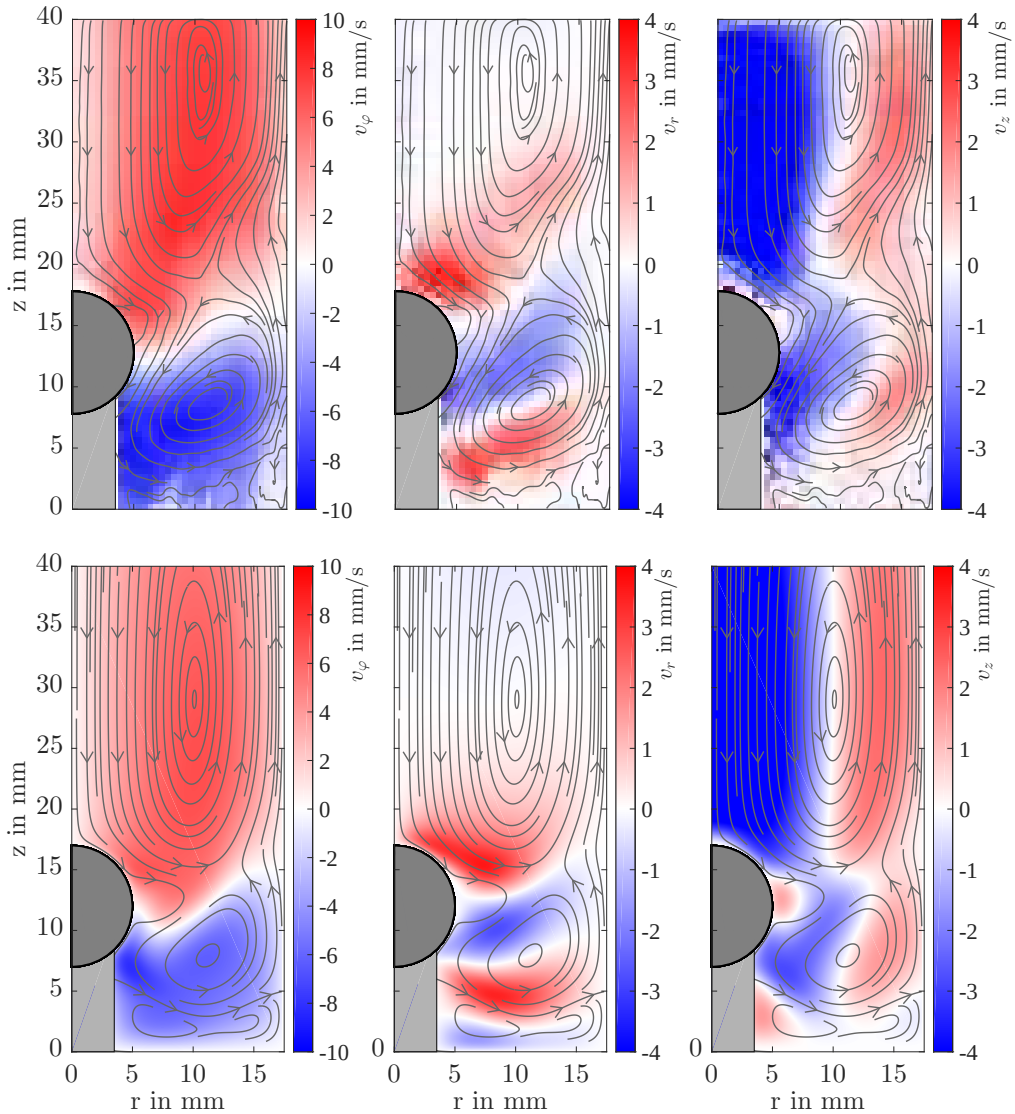

Figure 4: Experimentally (top) end numerically (bottom) obtained velocity field around the magnetized sphere in the rz-plane. The grid size for representation of the data is 0.5 mm and 0.25 mm in each direction for the experimental and numerical data, respectively. Circumferential velocity (left), radial velocity (middle) and axial velocity (right). The streamlines (grey) were added to better visualize the in-plane velocity field in the meridional (rz) plane.

meridional rz-plane together with stream lines of the secondary (in-plane) flow for the experiment (top) and the simulation (bottom). The azimuthal velocity v_φ is shown on the left, the radial velocity v_r in the middle and the axial/vertical velocity v_z on the right. As can be seen from the azimuthal velocity distribution (left side of Fig. 4), the experimental and numerical

data is in very good agreement. As expected, the Lorentz-forces give rise to a rotating flow with different sign on the upper and lower side of the sphere. This is different to the case of a microelectrode, where the Lorentz forces are dominant on the lower side of the bubble due to the high current density and no counter-rotating flow could be observed on the upper side [26]. Since the magnetized sphere is elevated, the bending of the electric field lines is in the same order of magnitude on both sides of the sphere and thus the Lorentz forces are also relatively similar in this case. In the region of the sphere ($8.5\,\mathrm{mm} \leq z \leq 18.5\,\mathrm{mm}$), the magnitude of the azimuthal flow above the sphere is indeed slightly larger ($\sim 10\%$) than in the lower part of the sphere as expected from the theoretical field distribution (Fig. 1). Furthermore, the average position of the shear layer between the counter-rotating flow regions is not horizontally aligned, but follows a curved path which is inclined upwards in radial direction and shows a minimum at $r = 7\,\mathrm{mm}$ and $z = 10\,\mathrm{mm}$. It can be also seen that the Lorentz-force-induced flow is not limited to the vicinity of the sphere but the fluid rotates in the entire cell due to viscous effects. Moreover, the azimuthal velocities increase with the applied current density as is shown on the right side of Fig. 5 for the maximum measured velocity in the cell. It can be seen that the maximum velocity increases approximately with the square root of the current density, $v_\varphi \sim \sqrt{j}$, which can be attributed to the fact that the dynamic pressure is directly related to the imposed Lorentz forces, i.e. $\frac{\rho}{2} v_\varphi^2 \sim jBd$ (d is the diameter of the sphere representing a characteristic length scale).

The azimuthal fluid motion will obviously give rise to centrifugal forces, which in turn will cause the pressure to increase toward the outer wall. Since the azimuthal velocity is the predominant flow component, the pressure change can be estimated by

$$\frac{\partial p}{\partial r} = \rho \frac{v_\varphi^2}{r}. \tag{11}$$

This is exemplified on the left side of Fig. 5, where the radial distribution of the azimuthal velocity and the corresponding relative pressure change are illustrated in a horizontal plane slightly above the sphere (numerical results). The relative pressure distribution obtained by integrating the velocity profile according to Eq. (11) is generally in good agreement with the distribution directly obtained from the numerical simulation. Differences occur within the inner region for $r < 5\,\mathrm{mm}$) directly above the sphere due to the action of the secondary flow as discussed below.

In the middle and right column of Fig. 4 the secondary flow in the meridional plane is shown and additionally highlighted by the streamlines. Due to the centrifugal force caused by the azimuthal motion above and below the sphere, the fluid is forced to move toward the outer part of the cell as indi-

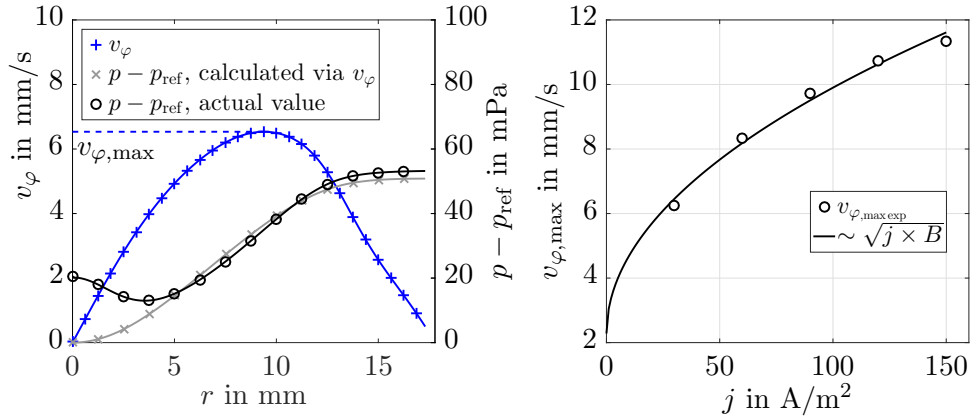

Figure 5: Radial distribution of v_φ and the relative pressure $p - p_{\mathrm{ref}}$ in a horizontal plane located 1 mm above the sphere obtained from the simulations at $j = 60$ A/m^2 (left). Maximum measured azimuthal velocity v_φ in the cell vs. the applied current density j (right).

cated by the red color in the representation of v_r. In the shear layer, where the azimuthal velocity and the centrifugal forces are rather small, the fluid flows back from the outer parts due to continuity. The numerical data shows that such inward directed flow is also evident close to the bottom of the cell. This can similarly be attributed to the low centrifugal momentum in the wall boundary layer which cannot withstand the elevated pressure in the outer cell region [see 38]. Since measurements close to the wall are subjected to a higher noise level, this effect cannot be seen in the experimental data.

The distribution of the axial velocity v_z is again in very good agreement between the experimental and numerical results. Above the sphere a large flow region is directed toward the sphere (indicated by the blue color, $v_z \approx$ -5 mms^{-1}). This is a consequence of the lower pressure in the center of the cell caused by the rotating motion. Due to the impingement of this flow on the upper part of the sphere the pressure reduction in this region is weaker compared to the case where only the action of azimuthal flow is considered as previously shown on the left side of Fig 5. After approaching the sphere the fluid is accelerated outwards due to the centrifugal forces as explained before. Finally, the fluid has to flow upwards at the outer part of the cell due to continuity. Since the available area becomes larger with increasing radius, the absolute velocity of the upward flow in the outer part is smaller ($v_z \approx 2$ mms^{-1}) compared to the downward flow in the inner part. It is also interesting to note that the portion of fluid moving downward along the sphere detaches from the sphere close to the equator at $r \approx 5$ mm and $z \approx 12$ mm, as indicated by the small region of upward moving motion. The

resolution of the experimental data is high enough to show the same feature, although to a smaller extent.

4.3. The hydrodynamic lift force

As suggested by Koza et al. [15] the higher azimuthal flow velocities on the upper side of the sphere will lead to a lower pressure in comparison to the lower side of the bubble. The result of such a pressure distribution is a hydrodynamic lift force that may facilitate the bubble detachment. However, as was shown before in Fig. 5 the pressure change induced by the azimuthal fluid motion is relatively small ($< 50\,\mathrm{mPa}$). By comparison, the hydrostatic pressure change around the sphere is $\Delta p = \rho g d \approx 100\,\mathrm{Pa}$. Thus, irrespective of the additional action of the secondary flow, the Lorentz-force-induced lift force can be expected to be several orders of magnitude lower than the buoyancy force. However, since the size of electrolytically generated hydrogen or oxygen gas bubbles is much smaller than that of the investigated sphere, it is important to understand how the respective forces scale with the diameter of the bubble. According to Eq. (11) the MHD-induced pressure change can be written as $\Delta p \sim \rho v_\varphi^2$. Moreover, the velocity scales approximately with $v_\varphi \sim \sqrt{jBd}$ as discussed before (see also Fig. 5, right). The MHD-induced pressure change can be therefore related to the Lorentz forces by

$$\Delta p \sim \rho v_\varphi^2 \sim jBd. \tag{12}$$

The resulting pressure-induced lift force can be then estimated according to

$$F_{\Delta p} \sim \Delta p \frac{\pi}{4} d^2 \sim jBd^3. \tag{13}$$

Thus, the generated lift force scales with d^3. Now, since the buoyancy of a gas bubble ($F_{Bz} \sim (\rho_l - \rho_g) g d^3$) also scales with d^3, the ratio between the lift force and the buoyancy force can be expected to be independent of the bubble size in a first approximation.

To support these findings, the imposed lift force can be directly calculated from the numerical simulations. To include the effect of the electrode on the Lorentz force distribution and the MHD flow, which was not correctly reproduced by the elevated magnetized sphere, the more realistic case of an insulating sphere directly attached to the electrode will be considered here. Fig. 6 shows the corresponding flow field, visualized by the three-dimensional streamlines colored by their velocity magnitude. In addition, pressure contours are shown in the meridional plane (rz-plane). The lift force $F_{\Delta p}$ calculated from this pressure distribution at different values of the sphere's diameter is shown on the right side of Fig. 6 together with the corresponding buoyancy force and the Reynolds number. The magnitude of the

simulated Lorentz forces was relatively small ($f_L \sim jB = 3.33\,\mathrm{Nm^{-3}}$), but still exceeds that used in the parallel fields experiment of Koza et al. [15] by about an order of magnitude. As can be seen, the hydrodynamic lift force $F_{\Delta p}$ is in the order of 10^{-7} N for a diameter of 10 mm and is approximately four orders of magnitude lower than the buoyancy force. As expected from the theoretical discussion, the $F_{\Delta p} \sim d^3$ dependency is generally evident. However, as the diameter is reduced the reduction of the lift force becomes even stronger due to viscous effect which become more relevant at low Reynolds numbers. Consequently, the MHD-induced lift force is unlikely to be the reason for the reduction of the bubble detachment diameter observed by Koza et al. [19, 20, 15] in an electrode-normal magnetic field.

On the other hand, for much higher current densities in the order of $10\,\mathrm{kAm^{-2}}$ and magnetic fields of $B \approx 1\,\mathrm{T}$ ($jB = 10\,\mathrm{kNm^{-3}}$), which are realistic conditions for practical applications, the lift force may have a more significant contribution. However, at high current densities the bubble coverage on the electrode surface and the void fraction becomes very high, so that the interaction between the bubbles would also have to be taken into account. In fact, even at low current densities and electrode bubble coverage the interaction between the MHD flow around the individual bubbles could lead to relevant flow effects as discussed in the next section.

4.4. Multiple magnets

In contrast to the MHD flow around single bubbles, the resulting MHD flow around a group of bubbles might give an alternative explanation of the earlier bubble release under magnetic field influence observed by Koza et al. [15]. Fig. 7 shows two different arrangements of nine cylindrical permanent magnets made of NdFeB (Fig. 7a, Fig. 7d) fixated below a 0.5 mm thick Pt foil used as cathode. A single magnet had a diameter and height both of $H = 3\,\mathrm{mm}$. The cell's diameter and height were 40 mm and 50 mm, respectively. The cell was filled with an aqueous solution of 0.9 M $CuSO_4$ and 1.5 M H_2SO_4. Current flows from a 10 mm high Cu anode mounted to the inner rim on top of the cell towards the cathodic Pt plate on the bottom of the cell. The arrangement is quite similar to the setup shown in Fig. 2. Since the magnetic fields of the upper poles of the permanent magnets penetrate the Pt foil circumferential Lorentz-forces are generated atop of each single magnet as sketched between Fig. 7b and Fig. 7c. Depending on the magnetization direction, the Lorentz-force is directed either clockwise (north pole on top) or counter-clockwise (south pole on top).

For the following discussion, a coordinate system originating at the cells center at the upper surface of the Pt foil will be used. z is the vertical coordinate. The flow was measured with conventional PIV in horizontal slices

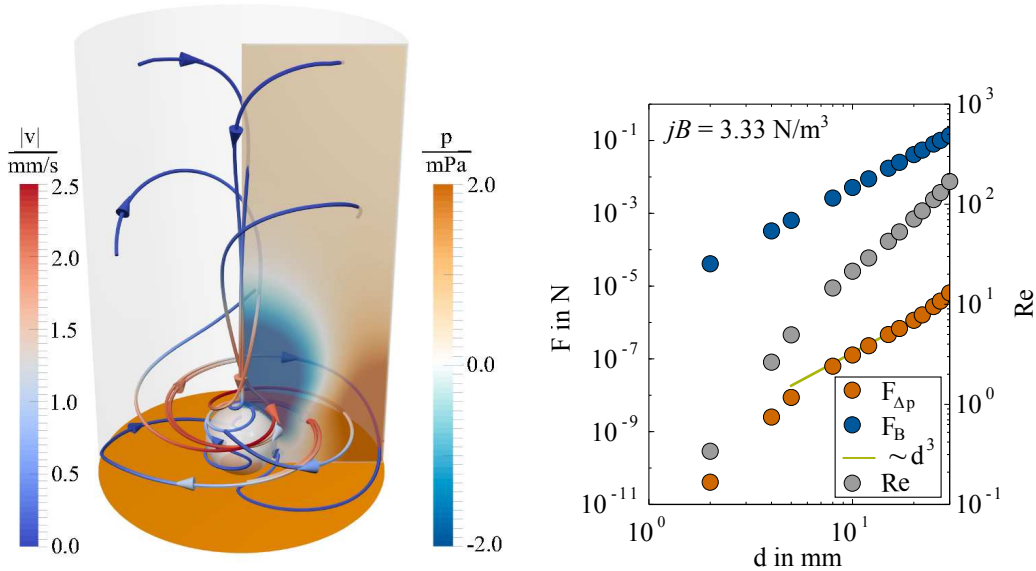

Figure 6: Rotating MHD flow around an insulating sphere obtained from numerical simulation with streamlines colored by the velocity magnitude and the pressure contour illustrated in the meridional plane (left). Hydrodynamic lift force, buoyancy and Reynolds number calculated for different diameters (right).

of constant z. Therefore, the velocity magnitude ($|v|$) contains only velocity components in the horizontal plane. In the checkerboard arrangement (Fig. 7a, b, e, f) the forces generated by the single magnets add up in the inter-magnet spaces. Accordingly, a relatively regular flow develops directly above the magnet array at $z = 1\,\mathrm{mm}$ (Fig. 7e) closely tracing the magnet contours. Slightly farther away from the cathode only a weak and barely detectable motion remains ($z = 5\,\mathrm{mm}$, Fig. 7f). Essentially, the checkerboard arrangement of the permanent magnets leads to a locally intense flow limited to the direct vicinity of the cathode. Further away some weak motions are still detectable, but no large scale flow is driven.

In contrast, an array of magnets with parallel magnetization directions (Fig. 7d) generates unidirectional rotation around the poles. In this case forces originating from the single magnets are opposing in the inter-magnetic spaces and partially cancel each other out (Fig. 7c). However, along the outer rim of the magnet array the Lorentz-forces from single magnets have the same (in the current case counter-clockwise) direction and add up. This situation is comparable to the summation of the magnetization currents in a volume, where only the surface magnetization currents contribute to the macroscopic field (c.f., e.g., [39]). The force configuration in Fig. 7d re-

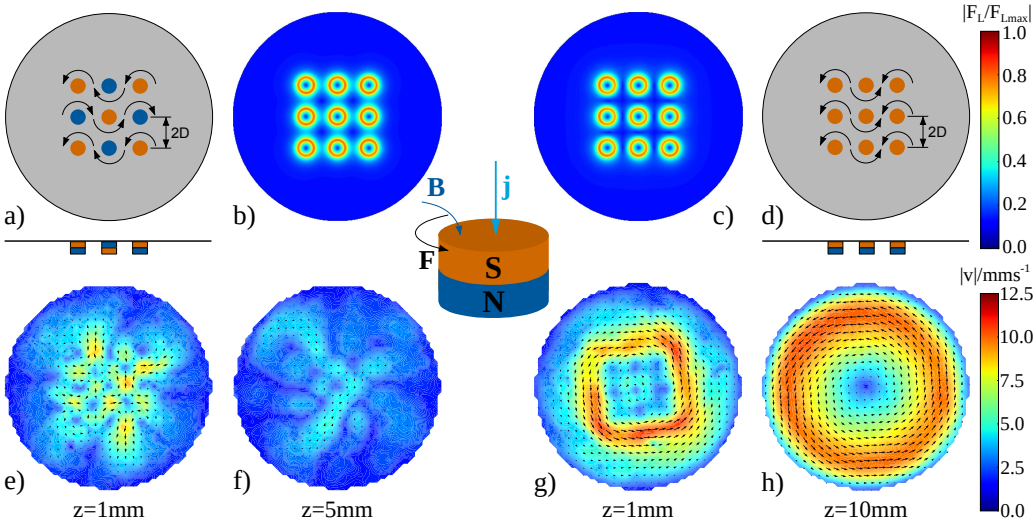

Figure 7: Lorentz-force distribution and flow generated by multiple magnets with magnetization directions all parallel (rightmost two columns) or in a checkerboard arrangement (leftmost two columns). A single magnet has a diameter $D = 3\,\mathrm{mm}$ and a height $H = 3\,\mathrm{mm}$, the cell diameter and height are 40 mm and 50 mm, respectively. Current densities of $380\,\mathrm{Am}^{-2}$ and $360\,\mathrm{Am}^{-2}$ were applied to the checkerboard (e, f) and the parallel (g, h) arrangement, respectively.

sembles that originating from a group of bubbles on a larger electrode. The direction of the azimuthal force around single bubbles is the same, so Lorentz-forces are weakened in the inter-bubble spaces but sum up around the bubble collective. Returning to the magnets, at $z = 1\,\mathrm{mm}$ (Fig. 7g) the electrolyte flows around the array following roughly the counter-clockwise Lorentz-forces along the eight outer magnets. The rectangular shape of the maximum velocity contour is tilted somewhat in flow direction with respect to the magnet array. Inside the array, velocities are much lower compared to those observed for the checkerboard pattern (c.f., Fig. 7e). In stark contrast to the checkerboard arrangement, the counter-clockwise Lorentz forces along the magnet array lead to an intense global flow spanning a large volume as can be seen from the horizontal cut at $z = 10\,\mathrm{mm}$ in Fig. 7h. Applied to multiple bubbles on an electrode this would mean that such a strong flow exerts drag forces on the bubbles acting mainly in electrode parallel direction. These drag forces could set the bubbles in sliding motion along the surface and support their earlier detachment.

5. Summary and conclusions

The aim of the current study was to investigate if the pressure change induced by the MHD flow in an electrode-normal magnetic field can significantly alter the detachment process of the bubble as hypothesized by Koza et al. [19, 20, 15]. Therefore, the complex three-dimensional flow around a magnetized sphere ($d = 10\,\mathrm{mm}$), mimicking an electrolytic gas bubble produced at a planar electrode was measured by astigmatism particle tracking. In order to gather the pressure information both the case of a magnetized sphere and an insulated sphere under the influence of a homogeneous magnetic field were investigated numerically.

The comparison between the numerical simulation and the experiment shows a very good agreement. Based on the numerical simulations, it could be shown that the MHD-induced lift force is to small to explain the accelerated bubble detachment observed by Koza et al. [15]. Moreover, it was theoretically and numerically shown that this lift force and the buoyancy force scale both with the bubble dimension to the third power. Thus the ratio of these forces and the conclusions remain the same even for very small hydrogen bubbles as present in real systems. On the other hand, experimental investigations of the flow generated by an array of magnets, representing a group of bubbles, show the generation of a significant global shear flow which may force an earlier bubble detachment and might therefore offer an explanation for the observations by Koza et al. [15].

6. Acknowledgements

The financial support from DFG through the Emmy-Noether Research group program under grant No. CI 185/3 is gratefully acknowledged by JM, DB and CC. The authors would also like to thank K. Eckert, M. Uhlemann, G. Mutschke und J. Koza for fruitful discussions. TW appreciates productive discussions with V. Galindo concerning OpenFOAM.

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